

GL Noble Denton

Aberdeen SMER Methodology

16th July 2012



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Content

- Background
- On-site Testing
- On-site Test Initial Results
- CFD Modelling
- Calculation of Error





- 21st July 2009 Problem was introduced at orifice plate change
- 27th July 2010 Orifice plate was changed but error persisted
- 7th August 2010 Fault initiated at Aberdeen AGI
 - Comparison of hourly volume (21 kscm) to line pack (32 kscm)
- 10th August 2010 Fault corrected
 - Incorrect counter reading (99950) was identified on orifice plate carrier
 - Orifice plate set to counter reading of 00000





- 21st July 2009 Problem was introduced at orifice plate change
 - ~30 kscm/h site flow prior to plate change
 - Fixed flow (30 kscm/h) recorded for duration of plate change
 - ~21 kscm/h site flow following plate change



Flow Profile 21st July 2009



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- 27th July 2010 Orifice plate was changed
 - Transient flow rate before and after plate change
 - No direct comparison available





- 10th August 2010 Fault corrected
 - ~20 kscm/h site flow prior to correction
 - Fixed flow (20 kscm/h) recorded for duration of correction
 - ~42 kscm/h site flow following correction



Flow Profile 10th August 2010



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- 5th August 2008 Correct orifice plate change
 - ~38 kscm/h site flow prior to plate change
 - Fixed flow (38 kscm/h) recorded for duration of plate change
 - ~38 kscm/h site flow following plate change



Flow Profile 5th August 2008



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- Counter reading at 99950 for July 2010 to August 2010
- Step changes suggest different counter reading for July 2009 to July 2010
- Most plausible counter reading for this period is 99985
 - Instruction plate on carrier includes 99885
 - Non-punched text is barely legible
 - 99885 relates to position in top chamber





On-site Testing

- Carrier Checks
 - Verified counter reading at correct location of plate
 - Measured position of plate relative to counter readings
 - Gathered some geometrical data from carrier
- Flow Tests
 - Pressure maintained by upstream party
 - Set FCV to fix flow rate
 - Positioned plate at various counter readings (removal and insertion)
 - Logged process data (DP, erroneous flow rate, etc)
 - Repeated for 3 different flow rates at 3 different pressures
 - Some instability in flow rate and pressure (pre- and post-check)



On-site Test Initial Results

- Flow Rate Instability
 - Linear correction applied to results for change in flow rates between start and end of testing
- Flow Test Results
 - Initial calculations indicate that the errors seem to be insensitive to pressure and flow rate at most points
 - Exception is low pressure, low flow rate points (which were successfully reproduced a second time)
 - Uncertainty levels increase rapidly at low differential pressures (low flow rates)



On-site Test Initial Results





CFD Modelling

- Dimensional data provided to independent CFD specialist to create model
- Known good process data provided to validate model
- Results produced for (incorrect) counter positions
- Model re-validated (if necessary) against unused flow test points
- Refined results produced for (incorrect) counter positions
- Results compared against on-site test results

Work completed

Work ongoing



Calculation of Error

- Comparison of on-site testing vs. CFD will determine methodology
- Good correlation will mean the CFD model can be used to predict errors at all pressure and flow rate combinations
- Poor or no correlation will mean the CFD model is inaccurate and cannot be used. On-site test data will be used to correct for errors
- Other If the CFD model agrees at certain points but not others then further on-site testing may be required



Calculation of Error

- Errors will be compared to step changes at orifice plate changes to support the suspected counter readings
- If error is found to be insensitive to pressure and flow rate then a single correction factor can be applied to the billed volumes for each period of the error. Indications from on-site testing are that this is the case.
- Dependency on pressure or flow rate will lead to correction of data on a 4minutely basis from the RBD data



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Thank you

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